

Thermodynamic Characterisation of Steel Corrosion for the Corrosion Inhibition of Steel in Sulphuric Acid Solutions by Artemisia

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Abstract

The effect of natural occurring extract of artemisia on the corrosion of steel in 0.5 M H₂SO₄ in the temperature range 298 – 353 K is studied by weight loss method, electrochemical polarisation and linear polarisation R_p measurements. Results obtained reveal that extract reduces the corrosion rate. The inhibition efficiency increases with the increase of artemisia content at 10 g/L to reach 95% and 99% at 298 and 353 K, respectively. Results obtained by gravimetric and electrochemical polarisation are in good agreement. Polarisation studies clearly reveal that the presence of the natural artemisia does not change the mechanism of the hydrogen evolution reaction and acts as a mixed type inhibitor. The inhibition efficiency increases with temperature. The adsorption of artemisia on the steel follows Langmuir adsorption isotherm.

Keywords: steel, artemisia, inhibition, corrosion, acid, natural substance.

Introduction

The most synthesised inhibitors used to secure metals against corrosion are generally a source of pollution hazards. The attempts to highlight environmentally friendly processes are reoriented to the use of natural products which are known as their environmental and acceptable ecological properties. Also, naturally occurring antioxidants are cheap and readily available and renewable sources of materials. Recently, many works show that they can be used as corrosion inhibitors; we cite natural honey [1], henna [2], occimum basclicum [3], ginger [4], extracts of fruits [5], thym [6], jojoba oil [7], rosemary

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oil [8, 9], eugenol [10]. Also, an extracted of an antibiotic and pyrrolidine alkaloids: bguanine is shown to be an efficient corrosion inhibitor of iron corrosion in 1 M HCl [11, 12].

In this optic, the encouraging results obtained by artemisia oil on the corrosion of steel in HCl [13] and H₃PO₄ [14] have incited us to test its extracts on steel corrosion in H₂SO₄. The literature shows that it received considerable attention as a promising and potent antimalarial drug for its stage specificity, its rather low toxicity. Literature shows that davanone (Fig .1) is the major constituent of artemisia herba alba in Morocco [15, 16]. Camphene, cineol-1,8, chrysanthenone, α and β -thujone and camphor are also detected. Recently, davanone has also the higher percentage (51.2%) in artemisia of Spanish origin [17] and Montenegro [18].

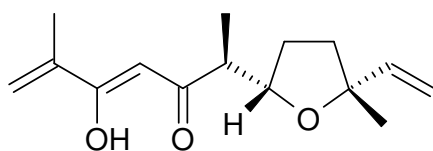


Figure 1. Molecular structural of davanone (249 g/mol).

The objective of the present paper is to study by gravimetric and polarisation methods the effect of extract of the natural artemisia on the corrosion of steel in 0.5 M H₂SO₄ solution. The effect of temperature between 298 and 353 K leads to the activation and adsorption of thermodynamic parameters.

Experimental details

Prior to all measurements, the steel samples (0.09 % P; 0.38 % Si; 0.01 % Al; 0.05 % Mn; 0.21 % C; 0.05 % S and the remainder iron) are polished with different emery paper up to 1000 grade, washed thoroughly with bidistilled water, degreased and dried with acetone.

The aggressive solution (0.5 M H₂SO₄) is prepared by dilution of Analytical Grade 98% H₂SO₄ with bidistilled water. 10 g of dried and powdered leaves of artemisia abyssinica are refluxed with 1 litre of 0.5 M H₂SO₄ at 373 K for 5 h. The extract was filtered from this stock solution from which solutions at different concentrations of the natural inhibitor are prepared.

Gravimetric measurements are carried out in double walled glass cell equipped with a thermostatic cooling condenser. One specimen is immersed in 100 cm³ of acid solution. The steel specimens used have a rectangular form (2 cm × 2 cm × 0.05 cm).

Electrochemical measurements are carried out in a conventional three-electrode electrolysis cylindrical pyrex glass cell. The temperature is controlled at 298 ± 0.5 K. The working electrode (WE) in the form of disc is cut from steel, has a geometric area of 1 cm² and is embedded in polytetrafluoroethylene (PTFE). A saturated calomel electrode (SCE) and a platinum electrode are used as reference and auxiliary electrodes, respectively. Running on an IBM compatible personal computer, the 352 Soft CorrTM III software communicates with EG&G

Instruments potentiostat-galvanostat model 263 at a scan rate of 20 mV/min. Before recording the polarisation curves, the steel electrode is polarized at -800 mV vs. SCE for 10 min. Polarisation curves are then recorded from -800 mV to anodic potentials. Values of linear polarisation resistance (R_p) are directly given by 352 Soft CorrTM III software obtained from the current potential plots. The test solution is de-aerated by pure nitrogen. Gas pebbling is maintained through the experiments.

Gravimetric and polarisation results obtained are deduced from the mean value of triplicate measurements.

Results and discussion

Weight loss measurements

The corrosion rate in 0.5 M H₂SO₄ (W_{corr}°) and at various concentrations of natural tested plant (W_{corr}) is determined after 6 h immersion. Values of corrosion rate and inhibition efficiencies are given in Table 1. The inhibition efficiency E_w , is determined by the relation:

$$E_w \% = 100 \times \left(1 - \frac{W_{\text{Corr}}}{W_{\text{Corr}}^{\circ}} \right) \quad (1)$$

where W_{corr} and W_{corr}° are the corrosion rates of steel in the presence and absence of artemisia, respectively.

Table 1. Gravimetric results of steel in acid with and without artemisia at various contents (t = 6 h).

Concentration (g/L)	W_{corr} (mg/cm ² .h)	E_w %
Blank	1.608	-
10 ⁻³	1.254	22
10 ⁻²	0.691	57
10 ⁻¹	0.418	74
1	0.209	87
10	0.081	95

The addition of artemisia reduces the corrosion rate in H₂SO₄ solution. The inhibitory effect increases with the increase of artemisia concentration. E_w reaches a maximum of 95% at 10 g/L for artemisia. This result shows that artemisia extract is a good inhibitor of steel corrosion in 0.5 M H₂SO₄ solution.

Polarisation measurements

Polarisation behaviour of steel in 0.5 M H₂SO₄ in the presence and absence of artemisia is shown in Fig. 2. Table 2 gives values of corrosion current density (I_{corr}), corrosion potential (E_{corr}), cathodic Tafel slope (b_c), anodic Tafel slope (b_a), and polarisation resistance (R_p). The inhibition efficiency (E_I %) is calculated by the relation:

$$E_I (\%) = \left(1 - \frac{I_{corr}}{I_{corr}^0}\right) \cdot 100 \quad (2)$$

where I_{corr}^0 and I_{corr} are the uninhibited and inhibited corrosion current densities, respectively, determined by extrapolation of cathodic Tafel lines to corrosion potential.

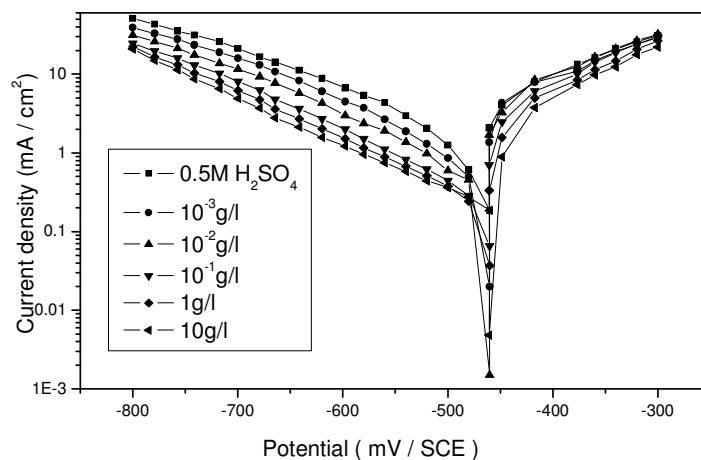


Figure 2. Polarisation curves of steel in H_2SO_4 at various concentrations of artemisia at 298 K.

Table 2. Electrochemical parameters of steel in 0.5 M H_2SO_4 + artemisia at various concentrations.

Concentration (g/L)	E_{corr} (mV/SCE)	β_c (mV/dec)	β_a (mV/dec)	I_{corr} ($\mu A/cm^2$)	E_I (%)	R_p (Ω/cm)	E_R (%)
Blank	-474	166	52	552	-	31	-
10^{-3}	-463	143	61	440	20	42	25
10^{-2}	-472	127	61	285	48	63	51
10^{-1}	-471	151	57	169	69	106	71
1	-474	150	47	66	88	206	85
10	-473	171	68	50	91	517	94

As it is shown in Fig. 1 and Table 2, cathodic polarisation curves rise to parallel Tafel lines indicating that the hydrogen evolution reaction is control activation. Thus the presence of natural artemisia does not affect the mechanism of this process. The addition of natural substance causes a decrease of the current density. Values of E_{corr} and cathodic Tafel slope (β_c) do not change when the concentration increases. The results demonstrate that the hydrogen reduction is inhibited and that the inhibition efficiency increases with inhibitor concentration to reach a maximum value of 91% at 10 g/L of artemisia.

In the anodic range, the polarisation curves of steel in 0.5 M H₂SO₄ with and without artemisia show that the presence of inhibitor decreases the current density. This fact means that artemisia inhibits anodic reaction and acts as a mixed type inhibitor.

The corresponding polarisation resistance (R_p) values of steel in 0.5 M H₂SO₄ in the presence and absence of different concentrations of the inhibitor are also given in Table 2. The inhibition efficiency E_R% is calculated as follows:

$$E_R \% = 100 \cdot \left(1 - \frac{R_p}{R_p'}\right) \quad (3)$$

where R_p and R_p' are the polarisation resistance with and without the inhibitor, respectively.

We remark that R_p increases with increasing the inhibitor concentration. This in turn leads to a decrease in I_{corr} values. The efficiency increases with the product content and attains 94%.

Effect of temperature

The influence of temperature on the corrosion behaviour of steel/acid added of artemisia at various concentrations is investigated by weight-loss trends in the temperature range 298-353 K during 1 h of immersion. The variation of the inhibition efficiency of artemisia with temperature is shown in Fig. 3. E% increases with temperature to attain 99% at 353 K.

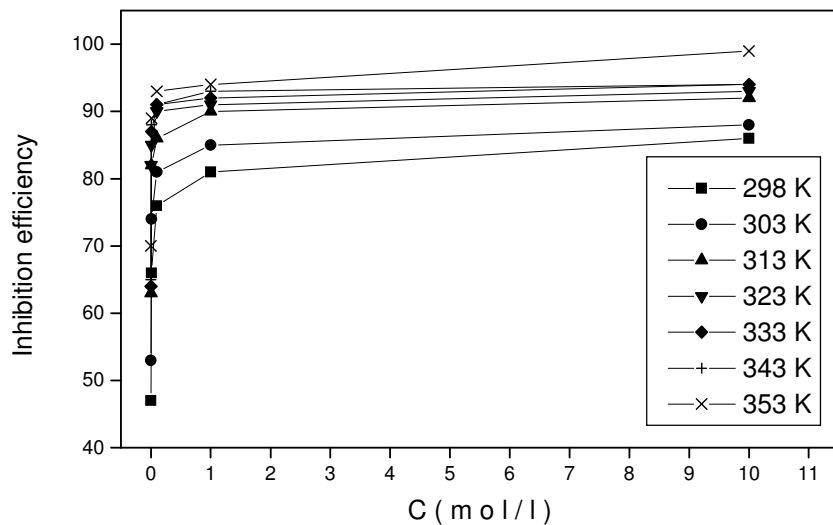


Figure 3. Evolution of efficiency at various concentrations of artemisia at different temperatures.

The activation energy can be determined from Arrhenius plots for steel corrosion rate presented in Fig. 4 by the following relation:

$$W = K \cdot \exp(-E_a/RT) \text{ and } W' = K \cdot \exp(-E_a'/RT) \quad (4)$$

where E_a and E_a' are the apparent activation energies for the corrosion in the absence and presence of the inhibitor at different concentrations, respectively. It is obvious that the activation energy of the inhibited solution in this study decreases by increasing the concentration of artemisia. The increase of $E\%$ and decrease of E_a are generally regarded as chemisorption [19, 20]. For calculating the entropy ΔS^* and enthalpy ΔH^* of activation, the alternative formulation of the Arrhenius equation is the transition state equation [21-23]:

$$W = \frac{RT}{Nh} \exp\left(\frac{\Delta S^*}{R}\right) \exp\left(-\frac{\Delta H^*}{RT}\right) \quad (5)$$

being h the Plank's constant, and N Avogadro's number.

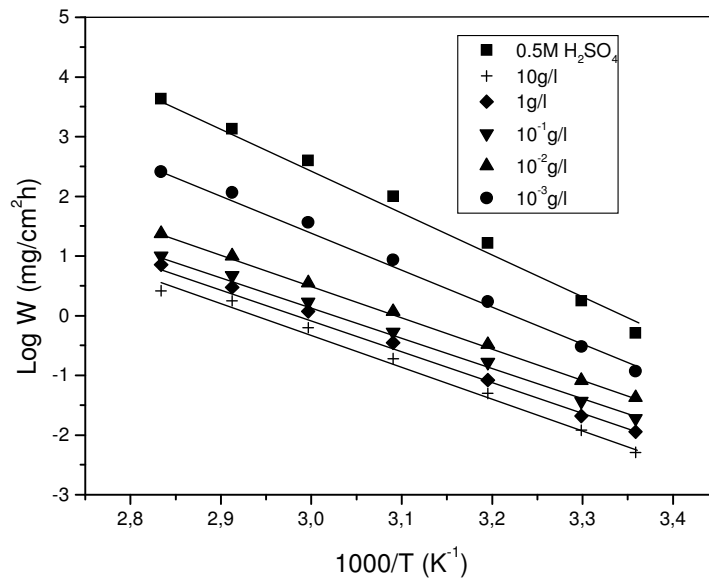


Figure 4. Arrhenius plots for the dissolution of steel in 0.5 M H_2SO_4 in the absence and presence of artemisia.

Fig. 5 shows straight lines of plots of $\text{Log}(W_{\text{corr}}/T)$ vs. $1/T$ with a slope of $\Delta H^*/R$ and an intercept of $(\text{Log}(R/Nh) + \Delta S^*/R)$. Values of E_a , ΔH^* and ΔS^* are collected in Table 3. The data show that the thermodynamic parameters (ΔH^* and ΔS^*) of the dissolution reaction of steel in 0.5 M H_2SO_4 in the presence of artemisia are lower than those of the non-inhibited solution. The positive values of ΔH^* suggest that the dissolution process is an exothermic phenomenon and that the dissolution of steel is difficult. Also, the entropy ΔS^* widely decreases with the content of the inhibitor. This means the formation of an ordered stable layer of inhibitor on the steel surface [24].

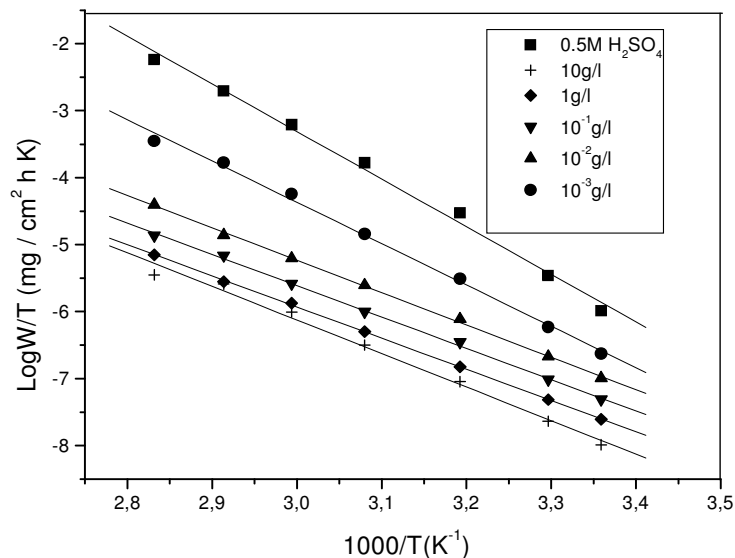


Figure 5. Plots of Log (W/T) vs. 1/T for steel in different additives of artemisia.

Table 3. Activation parameters of steel in 0.5 M H₂SO₄ with and without artemisia.

Concentration (g/L)	E _a (kJ.mol ⁻¹)	ΔH* (kJ.mol ⁻¹)	ΔS* (J.mol ⁻¹ K ⁻¹)
Blank	61.83	59.15	-47.75
10 ⁻³	54.08	51.37	-79.88
10 ⁻²	43.98	40.21	-12055
10 ⁻¹	43.81	38.93	-127.56
1	45.40	38.71	-130.87
10	44.42	37.42	-137.87

Adsorption isotherm

Fig. 6 shows the linear dependence of C/θ as a function of C, where θ is the surface coverage determined by the ratio E%/100. The inhibitor adsorbs on the steel surface according to the Langmuir kind isotherm model by the relation [25]:

$$\frac{C}{\theta} = \frac{1}{K} + C \quad \text{with} \quad K = A \exp\left(\frac{-\Delta G_{ads}}{RT}\right) \quad (6)$$

where K is the equilibrium constant of the adsorption process.

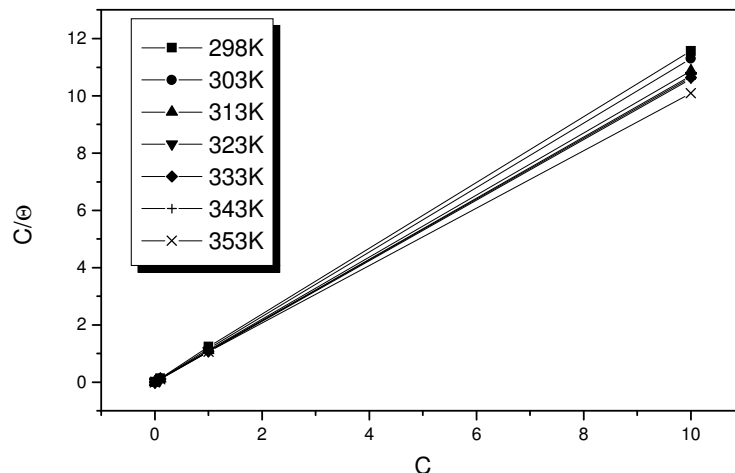


Figure 6. Langmuir's adsorption isotherm model for artemisia in 0.5 M H₂SO₄ at different temperatures.

Thermodynamic model is a good tool to explain the adsorption phenomenon of the inhibitor molecule. ΔH_{ads} may be determined from the Van't Hoff equation [26-27]:

$$\ln K = -\frac{\Delta H_{ads}}{RT} + Constant \quad (7)$$

where ΔH_{ads} and K are the adsorption heat and adsorptive equilibrium constant, respectively.

Fig. 7 is the straight line $\ln K \sim 1/T$. The adsorption heat (ΔH_{ads}) can be approximately regarded as the standard adsorption heat (ΔH_{ads}) under the experimental conditions [27-28].

Then the standard adsorption entropy ΔS_{ads} can be obtained by the thermodynamic basic equation $\Delta G_{ads} = \Delta H_{ads} - T\Delta S_{ads}$ (Fig. 8). Data obtained from this figure are $\Delta H_{ads} = 24.14$ kJ/mol and $\Delta S_{ads} = -194.3$ J/mol.K. Adsorption equilibrium constants K and other thermodynamic parameters for the adsorption process are listed in Table 4.

The negative value of ΔG_{ads} means that the adsorption of artemisia extract on steel surface is a spontaneous process, and furthermore the negative values of ΔG_{ads} also show the strong interaction of the inhibitor molecule onto the steel surface [29, 30].

It was found that ΔG_{ads} increases negatively with increasing the temperature; this phenomenon once again indicates that the adsorption is favourable with increasing experimental temperature and dominates on the desorption of the inhibitor from the steel surface.

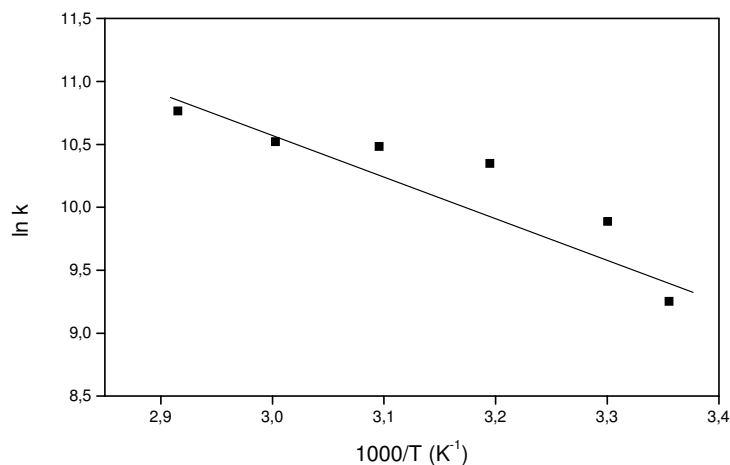


Figure 7. Relationship between $\ln K$ and $1/T$.

The values of thermodynamic parameters for the adsorption of inhibitors can provide valuable information about the mechanism of corrosion inhibition. The endothermic adsorption process ($\Delta H_{\text{ads}} > 0$) is attributed unequivocally to chemisorption [31], while generally, an exothermic adsorption process ($\Delta H_{\text{ads}} < 0$) may involve either physisorption or chemisorption or a mixture of both the processes. In the present case, the positive sign of $\Delta H_{\text{ads}}^{\circ}$ (24.44 kJ/mol) indicates that the adsorption of inhibitor molecules is an endothermic process [32]. The positive values of ΔS_{ads} indicate that the adsorption is a process accompanied by an increase in entropy. Therefore, the values of ΔH_{ads} and ΔS_{ads} obtained by both methods are in good agreement.

Table 4. Thermodynamic data for studied artemisia from experimental adsorption isotherm.

T (K)	Slope	k	ΔG_{ads} (kJ/mol)	ΔH_{ads} (kJ/mol)	ΔS_{ads} (J mol ⁻¹ k ⁻¹)
298	1.15	10438,08	-32.9	24.44	192.42
303	1.12	19646,1	-35.0	24.44	196.17
313	1.08	31199,7	-37.4	24.44	197.57
323	1.06	35656,8	-39.0	24.44	196.40
333	1.06	37051,2	-40.3	24.44	194.41
343	1.05	47310	-42.2	24.44	194.86

The values of ΔG_{ads} are negative indicating that natural substance is strongly adsorbed on the metal surface [33]. Furthermore ΔG_{ads} becomes more negative with the rise of temperature showing the high protection of natural plant at 353 K (99%).

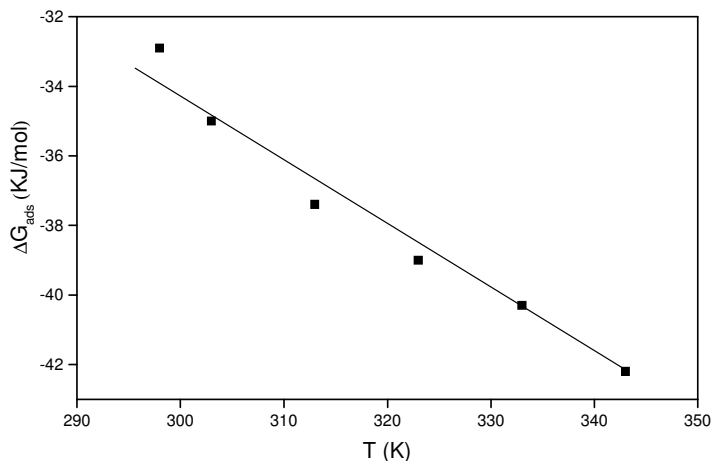
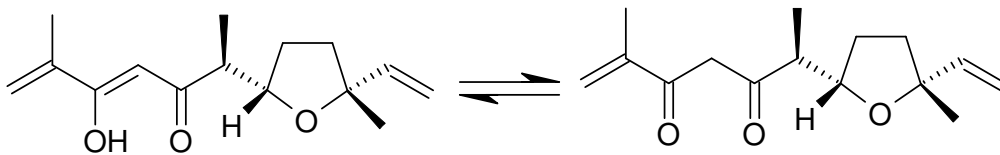
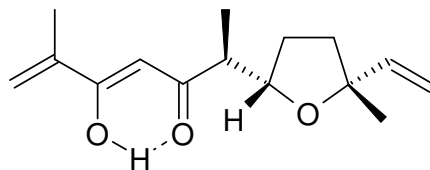


Figure 8. Variation of ΔG_{ads} with temperature.

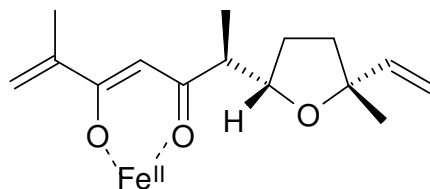
The adsorption phenomenon of davanone of oil may be explained by tautomeric equilibrium:



And also the davanone molecular may be stabilized by intramolecular hydrogen bond which enhances efficiency. Such results were obtained by other works [33].



Since davanone is a diketone compound, the inhibitory action may be also interpreted by the formations of Fe(II)-davanone complex as recently shown in the literature [34].



Conclusion

- Artemisia extract acts as a mixed type inhibitor for the corrosion of steel in 0.5 M H₂SO₄ without modifying the mechanism of hydrogen evolution reaction.
- The polarisation resistance increases with the content of the inhibitor.
- The adsorption of artemisia on the steel surface in sulphuric acid obeys to the Langmuir adsorption isotherm model.
- The inhibition efficiency of artemisia increases with the temperature and the activation corrosion energy decreases in presence of the inhibitor.
- Gravimetric, electrochemical and polarisation resistance measurements are in good agreement.

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